

# Synthesis of SAPO-41 from a new reproducible route using $\text{H}_3\text{PO}_3$ as the phosphorus source and its application in hydroisomerization of *n*-decane

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## Abstract

In the new reproducible route, phosphorous acid ( $\text{H}_3\text{PO}_3$ ) or the mixture of  $\text{H}_3\text{PO}_3$  and phosphoric acid ( $\text{H}_3\text{PO}_4$ ) are used as the phosphorus source to synthesize microporous silicoaluminophosphates. It is found that gels containing  $\text{H}_3\text{PO}_3$  favor the formation of SAPO-41 materials. With only  $\text{H}_3\text{PO}_3$  as the phosphorus source, pure SAPO-41 phase can be prepared with high crystallinity. When the mixture of  $\text{H}_3\text{PO}_3$  and  $\text{H}_3\text{PO}_4$  is used as the phosphorus source, the crystallization of SAPO-41 can be accelerated. Raman and XRD results show that SAPO-41 can be formed after crystallizing for 12 h. The dosage of the template di-*n*-propylamine (DPA) can be reduced in the mixed phosphorus source system. The SAPO-41 has been used to prepare catalysts for the hydroisomerization of *n*-decane. High selectivity of isomerization (89.5%) has been observed even at high conversion (88%) over the Pt/SAPO-41.

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**Keywords:** Phosphorous acid ( $\text{H}_3\text{PO}_3$ ); Mixed phosphorus source of  $\text{H}_3\text{PO}_3$  with  $\text{H}_3\text{PO}_4$ ; SAPO-41; Raman; *n*-Decane hydroisomerization

## 1. Introduction

Hydroisomerization of *n*-paraffins is of considerable interest and plays an important role in the petroleum industry to improve the octane number of gasoline and to increase the low temperature performance of diesel. Catalysts based on molecular sieves with monodimensional non-insecting and medium-pore channels have displayed high selectivity for the task [1–3]. In the family of silicoaluminophosphates, a process for lube dewaxing based on SAPO-11 has been developed [4,5]. It is notable that SAPO-41 has the pore size with  $0.70 \text{ nm} \times 0.43 \text{ nm}$  and shows very high efficiency for the selective hydroisomerization of long chain alkanes comparing with SAPO-11 (with the pore size  $0.39 \text{ nm} \times 0.63 \text{ nm}$ ) and SAPO-31 (with the pore size  $0.54 \text{ nm} \times 0.54 \text{ nm}$ ) [6]. However, in conventional synthesis route from gels containing phosphoric acid, reactive alumina, silica and organic template di-*n*-propylamine, the pure phase of

SAPO-41 is difficult to be reproduced and readily crystallize along with other DPA-templated structures such as SAPO-11 or SAPO-31. Many works contributed to the synthesis of the pure SAPO-41 and AIPO-41 materials have been done in the past few years [7–10]. However, the existence of some difficulties, such as demands of high template concentration, surfactant, high-purity grade reactants or longer crystallizing times, restricted the application of these materials.

Recently, several reports described the usage of non-conventional phosphorus sources. For example, by employing tributylphosphate as the source of phosphorus, several open-framework zinc and cobalt phosphates have been prepared hydrothermally.  $\text{Al}(\text{H}_2\text{PO}_4)_3$  or  $\text{H}_{10}\text{P}_8\text{O}_{25}$  have been used to the non-fluoride synthesis of triclinic form of  $\text{AlPO}_4$ -34, a CHA-structure type aluminophosphate molecular sieve which has never been synthesized previously in the absence of fluoride ions. Non-conventional phosphorus sources may result in a system with distinct effects for the crystallization of phosphate-based molecular sieves [9,11,12]. The present work reported a new reproducible route to prepare SAPO-41 molecular sieve. By using  $\text{H}_3\text{PO}_3$  or the mixture of  $\text{H}_3\text{PO}_3$  and  $\text{H}_3\text{PO}_4$  as the

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P source in the presence of di-*n*-propylamine (denoted as DPA afterwards) as template, the pure SAPO-41 phase has been synthesized in aqueous system. The hydroisomerization of *n*-decane over these Pt/SAPO-41 catalysts showed high selectivity of isomerization (near 90%) even at high conversion (88%).

## 2. Experimental

### 2.1. Synthesis of SAPO-41

#### 2.1.1. $H_3PO_3$ as P source

Pseudoboehmite (2.21 g, water loss at 600 °C: 34.75 wt.%) was mixed with 10 g of deionized water.  $H_3PO_3$  solution (2.87 g of solid phosphorous acid dissolving in 10 g distilled water) was added dropwise to the above mixture to form a white paste. The mixture was stirred until it became homogeneous. Subsequently, 6.98 g of DPA were added dropwise under vigorous stirring. And then 0.6 ml aqueous silica sol (5.9 M  $SiO_2$ ) and 19.18 g of deionized water were added [13]. The typical molar composition of the reaction mixture is: 0.85  $Al_2O_3$ :2.0  $H_3PO_3$ :0.2  $SiO_2$ :4.0 DPA:95.4  $H_2O$ . The mixture was sealed in a Teflon-lined stainless-steel autoclave and heated at 200 °C under autogenous pressure. The products were filtered, washed with distilled water till pH 7 and then dried at ambient temperature. Table 1 lists the gel compositions and crystallization conditions for the formation of SAPO-41(A). It should be indicated that, the crystallization time in Tables 1 and 2 means the period for obtaining enough solid product to determine its phase and structure. The period of crystallization is from 5 to 9 days according to gel composition and crystallization conditions.

Table 1  
Gel compositions and crystallization conditions of SAPO-41

Sample	Reactant composition					Crystallization condition		Product
	$Al_2O_3$	$H_3PO_3$	$SiO_2$	DPA	$H_2O$	$T$ (°C)	$t$ (day)	
1	0.85	2.0	0.30	4.0	95.4	200	8	SAPO-43
2	0.85	2.0	0.20	4.0	95.4	200	9	SAPO-41
3	0.85	2.0	0.15	4.0	95.4	200	9	SAPO-41
4	0.85	2.0	0.10	4.0	95.4	200	9	SAPO-41
5	0.85	2.0	0.30	3.0	95.4	200	4	SAPO-47
6	0.85	2.0	0.20	3.0	95.4	200	7	SAPO-11
7	0.85	2.0	0.15	3.0	95.4	200	5	SAPO-11
8	0.85	2.0	0.10	3.0	95.4	200	7	SAPO-41

Table 2  
Gel compositions and crystallization conditions for SAPO-41 formation with the mixture of  $H_3PO_3$  and  $H_3PO_4$  as the P source

No.	Reactant composition						Crystallization condition	
	$Al_2O_3$	$H_3PO_3$	$H_3PO_4$	$SiO_2$	DPA	$H_2O$	$T$ (°C)	Time
9	0.80	0.66	1.33	0.20	2.67	33.33	200	2 days
10	0.80	1.33	0.66	0.07	2.67	33.33	200	4 days
11	0.80	0.66	1.33	0.07	2.67	33.33	200	19 h
12	0.80	0.33	1.67	0.07	2.67	33.33	200	12 h
13	0.80	0.66	1.33	0.07	1.67	33.33	200	2 days
14	0.80	0.66	1.33	0.07	2.67	63.3	200	4 days
15	1.00	0.66	1.33	0.07	2.67	33.33	200	2 days

#### 2.1.2. $H_3PO_3$ and $H_3PO_4$ as mixed P source

When the mixed P source of  $H_3PO_3$  and  $H_3PO_4$  were used,  $H_3PO_4$  was added following  $H_3PO_3$  according to the molar ratio in Table 2. Take an example (sample 9): 1.43 g of  $H_3PO_3$  was dissolved in 10 ml of distilled water, then 2.28 ml  $H_3PO_4$  was added slowly to  $H_3PO_3$  solution. After stirred for about half an hour, the mixture was added to 2.73 g of pseudoboehmite and then 29.18 g water was added in. The mixture was stirred for 2 h. Then 9.6 ml DPA was added in dropwise under vigorous stirring for 1 h. The typical molar composition of the reaction mixture is: 1.0  $Al_2O_3$ :1.0  $H_3PO_3$ :2.0  $H_3PO_4$ :0.2  $SiO_2$ :4.0 DPA:95.4  $H_2O$ . The mixture was sealed in a Teflon-lined stainless-steel autoclave and heated at 200 °C under autogenous pressure. Table 2 lists the gel compositions and crystallization conditions for the formation of SAPO-41.

### 2.2. Characterization

X-ray powder diffraction (XRD) patterns of the as-synthesized products were recorded on a Rigaku D/MAX-2500 diffractometer with Ni-filtered Cu K $\alpha$  radiation ( $\lambda = 1.5418 \text{ \AA}$ ). Raman spectra were determined by Renishaw inVia spectroscopy system. The laser used was Argon ion laser with 514.5 nm excitation source with power output of 20 mW. Element analysis was performed on a Elementar Varioel element analyzer. Thermal analysis was performed on Netzsch STA 409 PC thermal analyzer at a heating rate of 10 °C/min in nitrogen.

The acidity of the samples was characterized by temperature-programmed desorption of ammonia ( $NH_3$ -TPD).  $^{29}Si$  MAS NMR spectra were recorded at ambient temperature with a BRUKER-AM300 multinuclear spectrometer. Spin speeds

were ca. 5.5 kHz. The resonance frequencies observed were 79.5 MHz. Chemical shifts were recorded with respect to TMS for  $^{29}\text{Si}$ .

### 2.3. Preparation of Pt/SAPO-41

As-synthesized solid products of SAPO-41(A) were separated from the mother liquor by centrifugation and subsequently purified by a series of washing steps with distilled water, dried at  $120^\circ\text{C}$  for 2 h and then baked in air at  $300^\circ\text{C}$  for 1.5 h. Furthermore, the solid sample was calcined in air by heating at  $10^\circ\text{C}/\text{min}$  to  $550^\circ\text{C}$  for 10 h to remove the organic template completely. The composition of the calcined product was determined by inductively coupled plasma (ICP) spectroscopy. Pt/SAPO-41 catalysts were prepared by the incipient wetness impregnation technique. The required amount of an aqueous solution of  $\text{H}_2\text{PtCl}_4$  was added to the support at room temperature. The metal-loading samples were dried at  $110^\circ\text{C}$  for 2 h and calcined at  $500^\circ\text{C}$  for 4 h. Pt/SAPO-41 based on samples 9 and 11 in Table 2 are designated as SAPO-41-B1 and SAPO-41-B2, the  $\text{Si}/(\text{Si} + \text{P})$  in their framework were 0.09 and 0.05, respectively.

### 2.4. Catalytic reaction

The *n*-decane hydroisomerization was carried out in a fix-bed continuous flow reactor at atmospheric pressure. The catalyst powder was palletized, sieved to 20–30 mesh and 1.0 g of catalysts were loaded into the reactor. The sample was reduced at  $500^\circ\text{C}$  under hydrogen flow (35 ml/(min g)) for 2 h. After reduction, the temperature was lowered to reaction temperature. Liquid *n*-decane was pumped into vaporization, mixed with hydrogen at  $230^\circ\text{C}$  and fed to the reactor. The reaction products were collected and analyzed by gas chromatograph. The identification of products was done by GC–MS.

## 3. Results and discussion

### 3.1. Synthesis and characterization of SAPO-41

#### 3.1.1. Using $\text{H}_3\text{PO}_3$ as phosphorus source

Silica and template concentration in the gel have strong influence on the crystallization products. If the molar ratio of  $\text{SiO}_2/\text{H}_3\text{PO}_3$  is greater than 0.1 or  $\text{DPA}/\text{H}_3\text{PO}_3$  less than 1.5, SAPO-41 cannot be obtained. Also, there exists some correlation between silica and template concentration to prepare SAPO-41. Keeping other parameters constant, several DPA-templated SAPO molecular sieves have been obtained by varying silica and template concentration. At higher concentration of template ( $\text{DPA}/\text{H}_3\text{PO}_3 = 2.0$ ), SAPO-41 have been obtained at a wider range of silica content, the  $\text{SiO}_2/\text{H}_3\text{PO}_3$  molar ratio varying from 0.05, 0.08 to 0.10. When  $\text{DPA}/\text{H}_3\text{PO}_3$  decreased to 1.5, SAPO-41 has only been synthesized at  $\text{SiO}_2/\text{H}_3\text{PO}_3 = 0.05$ . ICP analysis show that silica contents in SAPO-41 increase with its feeding.

The powder X-ray diffraction (XRD) patterns of as-synthesized SAPO-41 are shown in Fig. 1. All the reflection

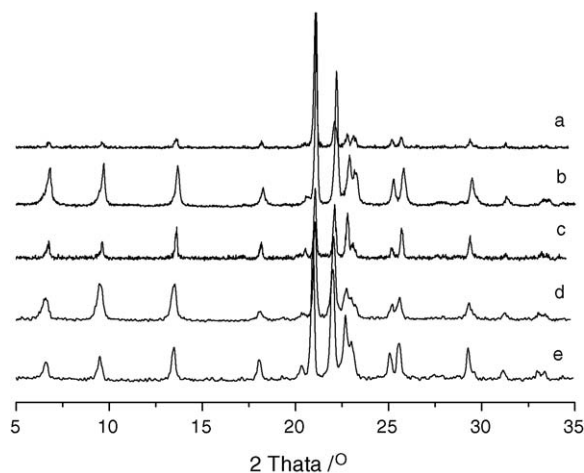


Fig. 1. XRD patterns of as-prepared SAPO-41 samples. (a) Sample 2, (b) sample 4, (c) sample 8, (d) sample 9 and (e) sample 11.

peaks of the products can be indexed as SAPO-41, which are in good agreement with the literature values of AFO structure [14]. No additional peaks are observed, which indicates that all the samples are free of impurities. However, the relative intensity of the peaks corresponding to the (2 1 1), (0 2 0) and (2 1 0) planes of sample 2 varied significantly from the literature values, which indicates the different tropism of the products [15].

#### 3.1.2. Using the mixture of $\text{H}_3\text{PO}_3$ and $\text{H}_3\text{PO}_4$ as phosphorus source

Pure SAPO-41 can be prepared by using  $\text{H}_3\text{PO}_3$  as the phosphorus source, but it needs a long time. In order to shorten the crystallization time, much effort has been done. Finally, a method by using  $\text{H}_3\text{PO}_4$  partly in place of  $\text{H}_3\text{PO}_3$  has been discovered.

It is notable that when  $\text{H}_3\text{PO}_4$  was introduced in the synthesizing procedure, the speed of SAPO-41 formation was accelerated remarkably (Table 2). With other conditions fixed, the crystallization period of SAPO-41 has been reduced from 7 to 9 days in the system  $\text{H}_3\text{PO}_3\text{--SiO}_2\text{--DPA--H}_2\text{O}$  to 2 days in the system  $\text{H}_3\text{PO}_4\text{--H}_3\text{PO}_3\text{--SiO}_2\text{--DPA--H}_2\text{O}$ . With the changes of  $\text{H}_3\text{PO}_4/\text{H}_3\text{PO}_3$  molar ratio from 0.5 to 2 and finally 5, SAPO-41 has even been obtained for about 12–20 h (samples 11 and 12 in Table 2). It is clear that it needs a certain time to perform the transformation of P(III) species to P(V). Introduction of  $\text{H}_3\text{PO}_4$  to the reaction mixture means reduction of the  $\text{H}_3\text{PO}_3$  content, so it will take shorter time for the gel to crystallize to SAPO-41.

Besides, by using the mixture of  $\text{H}_3\text{PO}_3$  and  $\text{H}_3\text{PO}_4$  as phosphorus source, the dosage of DPA for SAPO-41 formation decreased from  $\text{DPA}/\text{P} = 2.0\text{--}1.5$  with only  $\text{H}_3\text{PO}_3$  as the P source to 1.3. The molar ratio of  $\text{DPA}/\text{P}$  has even been decreased to 0.8 in Table 2 sample 13.

It has been known that the formation of open-framework structures is kinetically controlled and can be highly sensitive to the variation in reaction conditions such as the choice of solvent, pH and the nature of the metal source [16–19]. In the route using  $\text{H}_3\text{PO}_3$  as the P source, the formation of SAPO-41 as a preferable product may attribute to the transformation of P(III) species

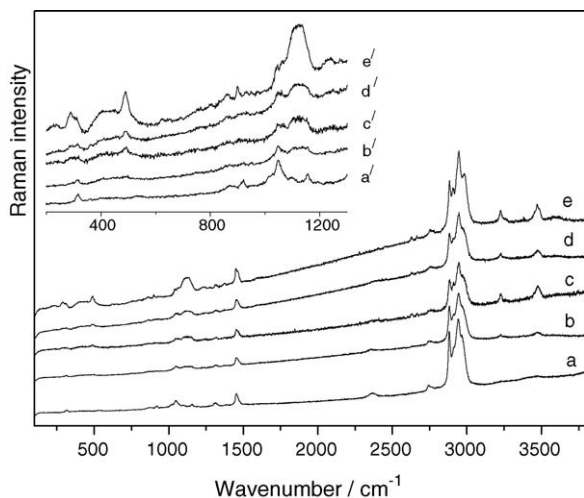


Fig. 2. Raman spectra of the solid gels obtained at various times during the crystallization of SAPO-41 (sample 10). (a)–(e) Correspond to crystallization time of 0, 12, 24, 48 and 72 h, respectively.

to P(V) species in the crystallization procedure. Fig. 2a–e and the corresponding insets a'–e' show the Raman spectra of the gels obtained as a function of time during the crystallization of SAPO-41 (sample 11). The assignment of the bands (Table 3) has been based on the special work of other researchers [20–26].

The first change in the Raman spectra that should be noted is in the region of  $2300\text{--}2400\text{ cm}^{-1}$ . This band is assigned to P–H vibration and is characteristic of  $\text{HPO}_3^-$ . It could be seen that the intensity of this band decrease during the first 12 h, and then disappear after 24 h, which means the P(III) species has transformed to P(V). The initial gel showed Raman bands at  $316, 869, 951, 1014$  (should),  $1026$  (should),  $1047, 1097$  and  $1156\text{ cm}^{-1}$  in the region of  $200\text{--}1300\text{ cm}^{-1}$ . During the crystallization process, some changes can be observed in the Raman spectra. These include decrease in intensity of the  $316\text{ cm}^{-1}$  band, appearance and sharpening of the  $289$  and  $491\text{ cm}^{-1}$  band, shift of  $921\text{ cm}^{-1}$  band to  $898\text{ cm}^{-1}$ , appearance and increase in intensity of the broad band around  $1121\text{ cm}^{-1}$ . The band at  $491\text{ cm}^{-1}$  is assigned to the motion of the framework oxygen atom in the plane perpendicular to the T–O–T band, and is correlated with the formation of even-numbered rings such as four-rings [25,26]. The band around  $1121\text{ cm}^{-1}$  correspond to the stretching vibration of P–O [21,22]. These two bands are first observed around 12 h, which suggests the formation of SAPO-41, and this is in agreement with XRD result. The band in the region of  $2700\text{--}3000$  and  $1448\text{ cm}^{-1}$  can be assigned to the C–H stretching and deforming vibration [20–22] of the template DPA.

Table 3  
Assignment of vibration bands [20–26]

Wavenumber ( $\text{cm}^{-1}$ )	Assignment
3479, 3226	O–H stretching vibration
2750–3000	C–H stretching vibration
2300–2450	P–H vibration
1448	Deformation vibration of $\text{CH}_2$
850–1200	P–O stretching vibration
350–550	Bending vibration of T–O–T

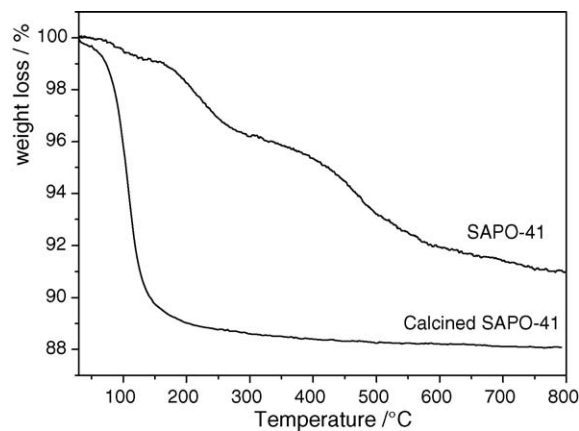


Fig. 3. TGA curves of as-prepared and calcined SAPO-41 (sample 11).

The TGA curve in Fig. 3 of as-prepared SAPO-41 (sample 11) exhibits three weight losses: the first one being about 0.85% occurring from  $50$  to  $140\text{ }^\circ\text{C}$  can be assigned to desorption of water molecules. The second weight losses about 2.92% occurring from  $140$  to  $310\text{ }^\circ\text{C}$ , and the third about 4.55% appearing between  $310$  and  $645\text{ }^\circ\text{C}$  are attributed to the elimination of the template and other organic molecules. TGA curve of SAPO-41 calcined as described in Section 2 exhibits only one weight loss around  $100\text{ }^\circ\text{C}$ , which suggests that the template in the pores of SAPO-41 has been completely removed.

### 3.2. Catalytic activity

#### 3.2.1. Acidity of SAPO-41

The catalytic performances of SAPO-*n* molecular sieves are strongly related to their acidity. The acidity of these materials result from the incorporation of silicon into the  $\text{AlPO}_4$  framework by silicon substituting only phosphorus (mechanism 2) or a phosphorus–aluminum pair (mechanism 3) [27,28].

$^{29}\text{Si}$  MAS NMR spectra and temperature-programmed desorption of ammonia  $\text{NH}_3$ -TPD patterns of SAPO-41 samples are shown in Fig. 4. For sample 11 with lower Si content, a resonance line centered around  $-91\text{ ppm}$  is observed, which can be ascribed to tetrahedral silicon atoms bound via oxygen to four aluminum atoms by the substitution mechanism 2 [27,6]. Each silicon atom incorporated in this way should produce a Bronsted acid site. For sample 9 with higher Si content, the additional line around  $-110\text{ ppm}$  is noted, which is assigned to Si atoms linked to neighboring Si atoms by the substitution mechanism 3. Substitution by mechanism 3 will generate much lower acidity than mechanism 2 [28]. So sample 11 should have more acid sites compared to sample 9.

It can be seen from the  $\text{NH}_3$ -TPD patterns that the amount of  $\text{NH}_3$ -desorption of sample 11 is much more than that of sample 9, namely, the acid site number of sample 11 is about three times as that of sample 9. This is in accordance with the above result. The two samples with different Si content give a large peak at about  $210\text{ }^\circ\text{C}$ . This large peak can be assigned to weak acid sites formed by the substitution mechanism 2. For sample 9 with higher Si content, a small shoulder peak around  $320\text{ }^\circ\text{C}$



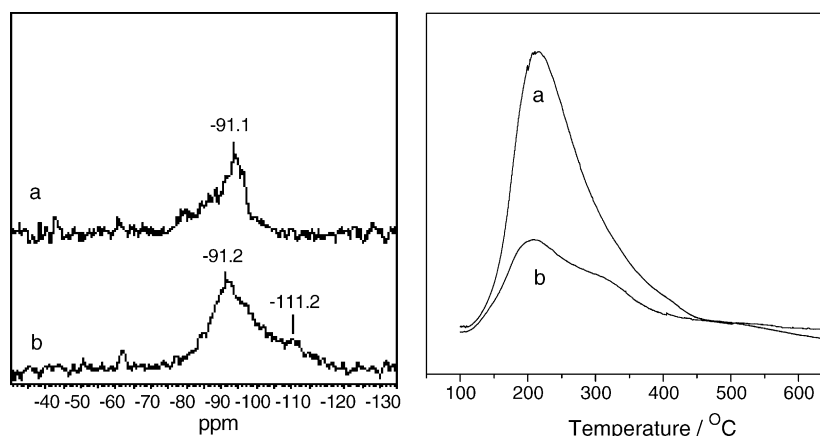


Fig. 4.  $^{29}\text{Si}$  MAS NMR spectra (left) and  $\text{NH}_3$ -TPD patterns (right) of SAPO-41: (a) sample 11 and (b) sample 9.

Table 4  
Results of *n*-decane hydroisomerization over SAPO-41 catalysts (in wt.%)

Reaction temperature (°C)	SAPO-41-B1				SAPO-41-B2			
	Conversion (%)	Selectivity of isomers (%)	Yield of isomers (%)	I/C	Conversion (%)	Selectivity of isomers (%)	Yield of isomers (%)	I/C
260	30.7	88.1	27.0	7.4	–	–	–	–
270	44.1	82.3	36.3	4.6	–	–	–	–
280	70.0	80.9	56.6	4.3	26.5	98.5	26.2	67.0
290	84.2	71.0	59.8	2.4	41.6	94.3	39.2	16.5
300	93.8	68.3	64.1	2.2	65.5	92.4	60.5	12.2
310	96.1	65.0	62.5	1.9	84.0	90.5	76.1	9.5
320	–	–	–	–	89.5	88.1	78.8	7.4
330	–	–	–	–	92.3	85.3	78.8	5.7
340	–	–	–	–	93.9	76.7	72.0	3.3

WHSV: 2/h;  $\text{H}_2$  flow rate: 35 ml/(min g); weight of catalyst: 1 g; time on stream: 0.5 h; I/C: isomers products/cracked products.

is observed, which is attributed to strong acid sites formed by the substitution of Si for Al and P pairs.

### 3.2.2. Catalytic performance of Pt/SAPO-41

Bifunctional Pt (0.5 wt.)/SAPO-41 catalysts based on samples 9 and 11, which have different Si content, were tested for the hydroisomerization of *n*-decane. The conversion of *n*-decane and isomers selectivity over Pt/SAPO-41 catalysts at 260–340 °C are shown in Table 4. The Pt/SAPO-41-B showed high isomer selectivity and high I/C value (ratio of isomers products/cracked products) for the hydroisomerization reaction of *n*-decane. High selectivity of isomerization (89.5%) was observed even at high conversion (88%) over Pt/SAPO-41-B2 catalyst. According to Meriaudeau et al. [6], the higher isomerization selectivity of Pt/SAPO-41 catalyst can be considered as a result of its pore dimension which varies the residence time of the reaction intermediates in the channels.

It can be seen from Table 4 that, to achieve high *n*-decane conversion, a higher reaction temperature is required over Pt/SAPO-41-B2 catalyst, which mean it has lower activity than Pt/SAPO-41-B1. But Pt/SAPO-41-B2 catalyst shows higher isomer selectivity and higher I/C value. Based on  $^{29}\text{Si}$  MAS NMR and  $\text{NH}_3$ -TPD analysis, acidity of sample 9 is stronger than sample 11, but the acid site number of sample 11 is greater than sample 9. It is believed that the higher *n*-decane conversion and

lower isomer yield over sample 9-based Pt/SAPO-41 catalyst is due to its strong acidity, while the higher isomer yield obtained over sample 11-based Pt/SAPO-41 is due to its suitable number of weak acid sites or suitable silicon content.

## 4. Conclusions

The present investigation describes the new route to synthesize pure AFO-type SAPO-41 in the presence of phosphorous acid ( $\text{H}_3\text{PO}_3$ ). It was found that, SAPO-41 can be obtained in a range of gel compositions, but the crystallization time was somehow as long as 5–9 days. When the mixed phosphorus source of  $\text{H}_3\text{PO}_3$  and  $\text{H}_3\text{PO}_4$  were used, the crystallization period of SAPO-41 can be shortened to 20 h–2 days. This is very important and useful for the application of SAPO-41 such as in the hydroisomerization of long-chain paraffin. The Pt/SAPO-41 showed high selectivity for the hydroisomerization of *n*-decane. High selectivity of isomerization (89.5%) was observed even at high conversion (88%) over Pt/SAPO-41-B2.

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